

COMPARISON REPORT: Final report

EURAMET Project 1508

Pilot study intercomparison of ultra-low liquid flow rates in range below 100 nL/min

February 2022

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1 – Introduction

This report was written as part of activity A1.3.5 from the EMPIR Metrology for Drug Delivery (MeDD II) project. The three-year European project commenced on 1st June 2019 and focused on providing traceable measurements of volume, flow and pressure of existing drug delivery devices and mixing behaviour and occlusion phenomena in multi-infusion systems. For more details about this project, please visit www.drugmetrology.com.

The aim of this comparison is to validate the developed primary standards for flow rates below 1500 nL/min for steady flow and for fast changing flow. This will allow the participating laboratories to test the agreement of their results and uncertainties despite the use of different equipment and calibration methods for the calibration of two different flow meters and a syringe pump.

NEL acted as the pilot laboratory by analyzing the data and producing the final report. METAS performed the initial and final measurements in this inter-comparison to test the stability of the flow meters over time and IPQ tested the stability of the CETONI Nemesys pump over time.

2 – Participants

The following Institutes have participated in this comparison

| no | Participant Type | Short Name | Organisation legal full name | Country |
|----|-------------------------|---------------|--|-------------------|
| 1 | Internal Funded Partner | NEL | TÜV SÜD National Engineering Laboratory | United Kingdom |
| 2 | Internal Funded Partner | IPQ | Instituto Português da Qualidade, I.P. | Portugal |
| 3 | Internal Funded Partner | СМІ | Cesky Metrologicky Institut | Czech Republic |
| 4 | Internal Funded Partner | METAS | Eidgenössisches Institut für Metrologie METAS | Switzerland |
| 5 | Internal Funded Partner | CETIAT | Centre Technique des Industries Aérauliques et Thermiques | France |
| 6 | Internal Funded Partner | RISE | RISE Research Institutes of Sweden AB | Sweden |
| 7 | Internal Funded Partner | DTI | Teknologisk Institut | Denmark |
| 8 | External Funded Partner | внт | Bronkhorst High-Tech BV | Netherlands |
| 9 | External Funded Partner | HS | Hahn-Schickard-Gesellschaft für angewandte Forschung e.V. | Germany |
| 10 | External Funded Partner | THL | Technische Hochschule Lübeck | Germany |
| 11 | External Funded Partner | UoS | University of Strathclyde | United Kingdom |

3 – Transfer standards

There were three transfer standards (TS) used in the inter-comparison exercise between the nine laboratories. Table 1 details the Transfer standard and flow range of the device during the comparison exercise.

| | Transfer Standard 1 [TS1] | Transfer Standard 2 [TS2] | Transfer Standard 3 [TS3] |
|----------------------|--|--|------------------------------|
| Manufacturer & model | Sensirion SLG64-0075 | Bronkhorst L01 | CETONI Nemesys |
| Type of device | Thermal flow meter | Thermal flow meter | Syringe pump |
| Flow range [nL/min] | 1500, 1000, 500, 100, 70, 50 and 20 | 1500, 1000, 500, 100, 70, 50 and 20 | 100, 50, 20, 10 and 5 |

| Table 1 – | Transfer standard | details |
|-----------|-------------------|---------|
|-----------|-------------------|---------|

All three transfer standards were used in the static tests, but only the thermal flow meters were used for the dynamic tests (Table 2).

| Table 2 – Type of | comparison | testing per | device |
|-------------------|------------|-------------|--------|
| | | 1001 | |

| | TS1 | TS2 | TS3 |
|---------------|-----|-----|-----|
| Static Tests | | | |
| Dynamic Tests | | | |

4 – Comparison schedule

The inter-comparison started in January 2021. The two flow meters and the syringe pump were shipped in separate boxes to shorten the dead laboratory time of each instrument. Each laboratory had 2 weeks for each instrument with an estimated Shipping period of 1 week. Each laboratory had a couple of weeks between each transfer standard to perform daily business work or improve the analysis of the data.

The following diagram illustrates the comparison schedule (Figure 1). METAS performed the initial and final measurements of the flow meters to test the flow stability over time. IPQ tested the flow stability of the CETONI Nemesys pump.

Bronkhorst High-Tech, L01-20D Sensirion AG, thermal SLG64-0075 CETONI Nemesys, syringe pump

| \$ | abDate | 18/01/20 | 1 25/01/20 | 1 01102/05 | 4 08/02/05 | 1 1510200 | 1 21020 | 1 01103/00 | 6103101 | 15103/01 | 2103/05 | 4 2103/01 | 6 00120 | 4 12/04/20 | 1 1910420 | 4 78/04/20 | 6 03/05/07 | 10105705 | 1 710540 | 4 24/05/201 | 4 31105/201 | SIDEEDY | AND BEAST | 2106/21 | 1 18106/10 1 | 1 15101720 | 1 12101700 | 4 191011207 | TENTION |
|---------|--------|----------|---------------|---------------|---------------|-----------|---------|---------------|---------|----------|---------|--------------|---------|---------------|-----------|---------------|---------------|----------|-------------|----------------|----------------|---------|-----------|---------|--------------------|---------------|---------------|----------------|---------|
| Week | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 | 20 | 21 | 22 | 23 | 24 | 25 | 26 | 27 | 28 | 29 | 30 | |
| METAS | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| IPQ | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| CETIAT | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| UoS/NEL | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| THL | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| HS | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| RISE | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| DTI | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| BHT-BV | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

Figure 1 – Comparison Schedule by laboratory for each comparison device

5 – Facility descriptions

This section of the report describes the participating laboratories and includes details of the methodology, measurement principle, fluids, flow ranges, operating conditions, and measurement uncertainty [1].

5.1 – Instituto Português da Qualidade (IPQ)



| | Figure 4. Satur for the Propherst mater calibration |
|--|---|
| | The syringe used was of 0.1 ml and 1 ml depending on the flow rate. |
| | Figure 5 - Setup for the CETONI Nemesys pump calibration The syringe used was of 0.01 ml and 0.1 ml depending on the flow rate. |
| Description of Measurement Principle | Interferometry Laser interferometry is used to measure the intensity of a wave resulting from the overlapping of two or more waves that have travelled over different distances and are superimposed on a single point therefore this methodology can be applied to measure the distance of the pusher block of a flow generator connected to a glass syringe to determine the flow rate. Model: $Q = v \times A = \frac{x_2 - x_1}{\Delta t} \times \pi r^2 = \frac{d\pi r^2}{t}$ |
| Facility Flow | Interferometry |
| Ranges | 1 mL/h to 0.0001 mL/h, <i>U</i> = 2% to 3 % |
| Temperature / Pressure Ranges | For all methods the temperature can go from 17 °C to 23 °C at atmospheric pressure. |
| Other Fluids | For all methods the primary fluid is water, but any other fluid can be used. |

| Uncertainty Budget | Interferometry |
|-----------------------|---|
| | The main standard uncertainties considered are: Distance (<i>d</i>), time (<i>t</i>), radius of the syringe (<i>r</i>), stability of the setup (δQ_{sta}), water temperature (<i>T</i>), time (<i>t</i>), expansion coefficient (γ), standard deviation of the measurements (δQ_{rep}) and repeatability of the 3 repetitions. |

5.2 – Centre Technique des Industries Aérauliques et Thermiques (CETIAT)



| Temperature / Pressure Ranges | Liquid flow temperature is controlled at +/-1°C from 10°C to 50°C, as the device under test and/or the flow generator (depending on the calibration conditions needed) is placed inside a climatic chamber. |
|-------------------------------------|---|
| Other Fluids | Measurements are carried out using ultra-pure water flowing through the device under test. CETIAT degassed ultra-pure water properties are density of 998.2 kg/m3 at 20°C and conductivity of 0.06 μ S/cm. Other liquids can be used if necessary. |
| Uncertainty Budget | The different measured quantities in our system are: Inner diameter of the capillary tube, positions of the interface inside the capillary, timestamps corresponding to each interface position and velocity of the interface, to which are associated the following uncertainty components : 1-camera calibration and specifications, pixel intensity profile and digital image correlation methods for the diameter and position measurements, 2-frame rate calibration and exposure time for time measurements and 3- linear regression parameters for velocity. Additionally, the uncertainty budget includes the system's drift and temperature effect as well as the uncertainties corresponding to the correction of physical phenomena e.g., evaporation, thermal expansion, and stick-slip effect. |

5.3 – Eidgenössisches Institut für Metrologie (METAS)

Description of Facility The METAS Microflow and Milliflow facilities consist of homemade piston provers to generate the flow and the gravimetric method to determine the flow rate and calibrate the volumes and the volume flow rates of the piston prover. The flow generator, is filled with water and the water is pressed at the desired flow rate through the DUT and collected in the beaker on the balance, as shown in Figure 7.



Figure 7 – Schematic of the updated Microflow and the developed Milliflow facility at METAS. The METAS piston prover presses the water through the DUT in the beaker on the balance, where it is continuously collected. Other components are the pressure sensors, temperature sensors, pressure relief valve and the water reservoir

Weighing data are continuously collected by a real time system (RT), which communicates with the balance at 20 Hz via RS232. The weight value is directly paired with the time stamp of the RT. The other sensor values such as water pressure upstream and downstream of the DUT, the water temperature at various positions and the ambient conditions are recorded as well at a frequency of 1 Hz.

The position the piston prover is determined by counting the pulses sent by the linear measuring system by means of an FPGA, which is a Field Programmable Gate Array with hard coded program code running on a defined constant cycle time of the order of 25 ns (40 MHz). For each additional pulse in any direction, a time stamp of the FPGA is recorded and a pair with the position and the timestamp is formed. These pairs of values are then read from the main software at a lower frequency. The real time position is used to calculate the real time speed by means of linear least square fit over a time window that is adjustable. Multiplying the speed with the cross section of the piston gives the volume flow rate.

In the mode of fast changing flow rates, the data of the pressure sensors are collected with a FPGA and are paired with a timestamp. These pairs of data are also then read from the main software at a lower frequency. To synchronize the RT and the two FPGA-systems, a trigger signal is produced by one FPGA system and the other FPGA system is recording this trigger signal allowing a perfect match of the two timescales.



Figure 8 – METAS piston prover of the Microflow facility with a speed range from 0.1 mm/s to 0.1 μ m/s. (A) high precision linear stage, (B) linear measuring system, (C) syringe, (D) mounting syringe body, (E) mounting and positioning for syringe plunger. The same design and components are used for the METAS piston prover of the Milliflow facility, but with a different speed range from 4 mm/s to 4 μ m/s.



Figure 9 – Weighing zone on the balance of the Milliflow (left) and Microflow (right) facilities. (A) outlet needle, (B) beaker with cover, (C) glass filter, (D) water in evaporation trap, (E) mount for T and rH sensor, (F) balance, (G) tubing for humidity exchanger, (H) cover.



Figure 10 – Other measurement beakers for the Microflow facility. (left) beaker with glassfilter like the beaker for the Milliflow facility. (center and right) Capillary beaker, where the outlet needle is placed in the center of the capillary. Capillary beaker is suitable for the detection of fast changing flow rates.

| Description of Measurement Principle | Flow is generated by the piston prover. The real time position is used to calculate the real time speed by means of linear least square fit over a time window that is adjustable. Multiplying the speed with the cross section of the piston gives the volume flow rate. |
|--|--|
| | The gravimetric method consists of weighing the collected water in a beaker and applying several corrections such as evaporation, buoyancy correction, etc. The ambient conditions must be well controlled and recorded to avoid any virtual flow incident due to temperature instabilities in the absolute temperature and temperature gradients. |
| Can the Facility be | The facilities operate in static and dynamic mode. |
| used for Static / Dynamic or Both? | The facilities can produce dynamic or transient conditions (fast flow changes). The changes occur within a time of less than 1 second and a ratio of 1:500 can be obtained. The range of flow rates is set by the choice of the piston used. |
| | The gravimetric methods can detect these fast flow changes in the range of 400 mL/min down to 50 nL/min. |
| | The piston provers can generate these fast flow changes in the range of 400 mL/min down to 20 nL/min. |
| | Steady flow rates are also generated in the range from 400 mL/min down to 20 nL/min and measured by the gravimetric method in the range from 400 mL/min down to 50 nL/min. |
| | Volumes of the delivered liquid are determined either by the piston prover or the gravimetric method. |
| Facility Flow | Dynamic mode: 20 nL/min - 400 mL/min (Piston Prover) |
| hanges | Dynamic mode: 50 nL/min - 400 mL/min (Gravimetric Method) |
| | Steady mode: 20 nL/min - 400 mL/min (Piston Prover) |
| | Steady mode: 50 nL/min - 400 mL/min (Gravimetric Method) |
| Temperature | Temperature: ambient |
| Ranges | Pressure: 0 – 10 bar |
| Other Fluids | Primary fluid: distilled water |
| | Additional fluids: any non-harmful fluid |
| Uncertainty Budget | Dynamic mode: 20 nL/min (50 nL/min) - 400 mL/min, 2.0 % - 0.2 % |
| Duugei | Steady mode: 20 nL/min (50 nL/min) - 400 mL/min, 1.0 % - 0.07 % |
| | |

| Uncertainty components of the gravimetric method includes: |
|---|
| drift, calibration and reading uncertainty of the balance |
| uncertainty of linear least square fit |
| evaporation buoyancy correction |
| correction from conventional weight to real weight |
| stability of ambient temperature conditions |
| • stability of water temperature and temperature gradients at different positions along the piping (piston, DUT, Balance) |
| repeatability and stability of the flow detection |
| • stability of the capillary forces acting at the water bridge to the measurement beaker |
| Uncertainty components of the gravimetric method includes: |
| Linearity of the linear stage |
| Repeatability and stability of the flow generation |
| Influence of torque and force on the accuracy of the position of the plunger |
| |

5.4 - RISE Research Institutes of Sweden AB (RISE)



For further data acquisition a compactRIO DAQ system (cRIO-9040 with three expansion cards NI 9210, NI 9207 and NI 9216) from National Instruments is available.



| Description of Measurement Principle | Flow is generated by means of a syringe pump equipped with different syringes of various sizes. The desired flow rates can be adjusted by means of the syringe pump. | | | | | | | |
|--|---|--|--|--|--|--|--|--|
| | The weighing method is performed by collecting the water (or another liquid) in a beaker. The weighing scale is continuously read-out. After the measurements several corrections for evaporation and buoyancy effects, etc. are applied. | | | | | | | |
| | The measuring conditions in the laboratory (air pressure, room temperature and air humidity) are measured separately by means of a Vaisala PTU300 and various other (separate) sensors logged on RISE internal server (EXOscada). The Vaisala device has an internal data logger that can be read out via different interfaces. In addition, there is the possibility to connect the Vaisala device directly to the NI DAQ system compactRIO. The Vaisala device has current and voltage signal outputs for air temperature and air humidity. | | | | | | | |
| Can the Facility be | The facility can be operated in static and dynamic mode. | | | | | | | |
| used for Static / Dynamic or Both? | The facility can handle dynamic transient conditions (fast flow changes). The quantification of the change is mainly depended on the read-out of weighing scale used. In general, the weighing scale is read out at a higher frequency (up to 20 Hz) in the event of rapid changes. | | | | | | | |
| Facility Flow Ranges | The flow rate range of the test facility is 0.25 μl/h to 1 ml/h. | | | | | | | |
| Temperature / Pressure Ranges | Lab1: ambient temperature (around 23.5 ± 0.5 °C, climatic room) Lab2: ambient temperature (around 20.0 ± 0.5 °C, climatic room); limited access | | | | | | | |
| - | Pressure: 0 to 5 barg (upgradeable to max. 10 barg) | | | | | | | |
| Other Fluids | Primary fluid: ultra-pure and degassed water | | | | | | | |
| | Additional fluids: liquids other than water (non-toxic) | | | | | | | |
| Uncertainty Budget | Steady (static) flow: Target uncertainties: 0.5% (higher flow rates) to 5.0% (5 nL/min); lower flow rates on request | | | | | | | |
| | Unsteady (dynamic) flow: Target uncertainties: 0.5% (higher flow rates) to 5.0% (20 nL/min); lower flow rates on request | | | | | | | |

5.5 – Teknologisk Institut (DTI)

| Description of Facility | At DTI the primary standard covers a flow range from 100 ml/h (1.6 ml/min) to 1 μ l/h (17 nl/min) with uncertainties from 0.05 % to 5 % with calibration time from 10 - 75 min. The micro flow laboratory at DTI is accredited to a flow rate from 600 ml/h (10 ml/min) to 1 ml/h (17 μ l/min) with uncertainties from 0.05 % to 4 %. |
|----------------------------|---|
| | Design of the facility |
| | The setup is based on gravimetric measurements, i.e., the flow is determined from |
| | $Q = \frac{\Delta V}{\Delta t} = \frac{\Delta m / \rho_w}{\Delta t}.$ |
| | The time, Δt , is determined from an oscillator in order to make traceability feasible. The water density, ρ_w , is determined using a formula from literature and checked by measurements. The measuring beaker used is thoroughly cleaned and acclimatized to the balance. Demineralized degassed water is used as fluid. |
| | The most difficult parameter to determine accurately for small flow rates is the mass change, Δm . It is based on measurements made with a laboratory scale with microgram resolution. Several corrections are required, e.g., for buoyancy by air, displacement by the inlet ("needle"), evaporation, capillary forces and sticking. |
| | To allow for accurate weighing the entire setup is place on a granite table, which provides an almost vibration-free base. Furthermore, the temperature of the setup is stabilized. Rapid temperature variations are prevented by placing the entire setup in a custom-built isolation chamber. This chamber also minimizes draft and convection effects. The chamber consists of metal box which is shielded from the surroundings by an isolating layer. Long-term stability is ensured by the laboratory's climate control. |
| | Evaporation is dealt with in different ways depending on the flow rate. In the case of the smallest flows the evaporation is almost completely eliminated by covering the water by an oil layer (see below). Alternatively, evaporation can be limited by increasing the relative humidity near the beaker and/or reducing the reducing the opening aperture of the beaker. For small flow rates it may be needed to measure the evaporation rate regularly in order to reduce the resulting uncertainty. The liquid oil cover used as evaporation trap is very efficient as only an evaporation rate of < 9 nl/h is remaining. However, the water needs to be delivered below the oil surface through the outlet pipe, which leads to several challenges e.g., capillary forces, buoyancy, inertia, stiction and friction, absorption, adsorption, stick/slip, and vibration transferal. To limit these effects, the outlet pipe is made of 0.4 mm stainless steel tubing. |
| | The operational volume of the beaker is < 5 ml, yet the setup includes a system for emptying the beaker automatically when it becomes full. This system provides significant benefits for measurements at relative high flow rates, by reducing the amount of manual handling required and increasing the thermal stability of the setup. |
| | If the Device under test (DUT) is a flow meter, then the demineralized and degassed water runs from pump and into the DUT. For that purpose, three syringe pumps are installed. Two Cavro XLP 6000 pumps are working in parallel and used for flow rates > 50 µl/min, whereas a Cavro Centris pump is used for smaller values; the minimum rate for continuous flow is 1 µl/hr \approx 17 nl/min. In addition to steady flows the pumping system can also provide dynamic flow-rate profiles. |
| | If the DUT is a pump, the water exits the DUT and is lead to the scale via stainless steel tubing. This configuration has e.g., been used for some medical devices. |

Dynamic gravimetric weighing

The balance is connected to a computer, enabling measurements with a frequency of 10 Hz and traceable timestamps with a dedicated timing hardware. By having continuous read out it becomes possible to detect the actual flow rate as a function of time in contrast to the case of static weighing where the delivered mass is measured and divided by elapsed time. The resolution of the balance is 1 μ g, the output stability is below 10 μ g.



Figure 16 – Setup where the DUT is a syringe pump. Water is lead from the reservoir (1) through the degasser (2) and into the syringe pump (3). From the syringe pump water is lead to the balance (4) using stainless steel tubing. The outlet tube may be traversed through the oil-based layer and into the water in the beaker. The balance is connected to balance electronics (5) and to a PC. The setup is enclosed in a chamber (6). Flow meters are installed between pump (3) and scale (4).



Figure 17 – The syringe pumps are visible to the right, the flow meter (green) in the center and the weighing system to the extreme left. The height-adjustment system for the inlet and the six-port valve for the emptying system are located towards the left side between scale and flow meter. Different beakers are available depending on the flow rate. For this photo, the draft screen of the scale has been removed and the insolating box around the setup is opened.

Description of
MeasurementThe facility is based on the gravimetric principle with an optional oil layer in the beaker as
evaporation trap.Principle

| Can the Facility be used for Static / Dynamic or Both? | The scale can deliver data with a frequency of 10 Hz – and it seem suitable for measuring dynamic and transient conditions. In MeDD I the dynamic behavior of a syringe pump was measured/check on this setup. |
|--|---|
| Facility Flow Ranges | The maximum flow rate is 60 mL/hr (1 mL/min), if the automatic system for emptying the beaker can be employed (e.g., if the DUT is a flow meter). Otherwise, the maximum flow rate may be limited to 10 mL/hour (0.167 mL/min). The facility is tested (with success) for 5 μ L/hr (0.083 μ L/min), however a realistic aim is 1 μ L/hr (0.017 μ L/min). |
| Temperature / Pressure Ranges | The facility can only operate at ambient conditions, meaning room temperature in the lab (18 $^\circ C$ – 25 $^\circ C)$ |
| Other Fluids | Normally degassed demineralized water is used. However, it is also possible to use other fluids as well. Prior to the project insulin mimicking fluid has been tested. |
| Uncertainty Budget | The dominant uncertainty contribution (>90 %) for the setup comes from the uncertainties of the corrections for the forces between the outlet pipe, the water and oil in the measurement beaker. The measurement uncertainty is approx. 0.5 % (k =2) at the flow rate of 10 ml/h. Below flow rates of 300 µl/h the balance uncertainty and uncertainty of the correction for buoyancy become dominant (90 % at 5 µl/h), while the level of water rise within the beaker becomes insignificant (about 20 µm). The measurement uncertainty rises to about 5 % (k =2) at the lowest flow rate of 1 µl/h. |

5.6 – Hahn-Schickard-Gesellschaft für angewandte Forschung e.V. (HS)



| | particles, a light source, a camera to record a sequence of frames and a software to determine the flow velocity. | | | | | | | | | |
|---|---|--|--|--|--|--|--|--|--|--|
| | As a flow generation source, we used a syringe pump (CETONI Nemesys Low pressure). As medium for our Holo-PIV set-up, we use water with polyethylene beads (density: 0.989 g/cm^3 , diameter: $1-10 \mu \text{m}$). The channel's dimensions were $100 \times 300 \mu \text{m}$ (height x width). The sensor in the Holo-Setup has a pixel size of $1.67 \mu \text{m}$ and a frame rate of 3.2 fps . To prevent beads from getting into the device under test (sensor), we have inserted a filter (pore size: $0.45 \mu \text{m}$) in between. The filter was exchanged between each measurement to prevent clogging of the filter. | | | | | | | | | |
| | Sensor | | | | | | | | | |
| | Measurement Protocol: | | | | | | | | | |
| | • Prior each measurement the setup was set to rest 30-60 minutes to determine the zero-flow value | | | | | | | | | |
| | • Each flow rate was set for 30-60 minutes before the measurement was recorded | | | | | | | | | |
| | During the measurement 200 images were acquired | | | | | | | | | |
| | • During each measurement the temperature of the reservoir was determined | | | | | | | | | |
| | • The measurement points for each flow rate were repeated on different days at different times | | | | | | | | | |
| Can the Facility be used for Static / Dynamic or Both? | The described method could be used for static and dynamic measurements because it only depends on the framerate of the chosen camera. In this case, a camera with a framerate of 3.2 fps is used. Therefore, in theory dynamic changes in the range of 312.5 ms can be detected. | | | | | | | | | |
| Facility Flow Ranges | Flow range: 5 to 500 nl/min (planned) | | | | | | | | | |
| | Flow range: 60 to 6000 μl/min (current status) | | | | | | | | | |

| Temperature / Pressure Ranges | Pressure 0 to 2 bar | | | | | | | | |
|---------------------------------------|--|--|--|--|--|--|--|--|--|
| Other Fluids | If other fluids are used, the density of the beads has to be adapted (should be identical to prevent sedimentation). | | | | | | | | |
| Other Fluids Uncertainty Budget | If other fluids are used, the density of the beads has to be adapted (should be identical to prevent sedimentation). A detailed description of the uncertainty budget can be found in "2020-07-29-MeDD_II A1.2.1 Report Template_microPIV". The main components of the facility uncertainty are: • Effective resolution of optical setup • Angular deviation of camera and flow channel (width b and height a) from 90° • Channel fabrication errors The combined uncertainty can be calculated as: $\frac{u_c(Q)}{Q} = \sqrt{\left(\frac{1.67\mu m}{\Delta x}\right)^2 + (1.37 \times 10^{-3})^2 + \left(\frac{3\mu m}{a}\right)^2 + \left(\frac{5\mu m}{b}\right)^2}$ Given that: $\Delta x = \frac{Q \times \Delta t}{a \times b}$ With: $a = 100\mu m$ $b = 300\mu m$ $\Delta t = \frac{1}{3.2s}$ This enables the calculation of the combined uncertainty as a function of the reference flow rate: Combined Uncertainty (UC) vs Reference Flow Rate (Q) -Uc (W) - Uc (Winnin) | | | | | | | | |
| | | | | | | | | | |
| | g_{g}^{0} f_{g}^{0} f_{g | | | | | | | | |

5.7 – Bronkhorst High-Tech BV (BHT)

Description of At the Bronkhorst facility the primary reference for mass flow is a high precision balance. Facility The primary standard covers flow calibrations in 2 ranges: (1) 1–2000 [mg/h] mass flow of water $(20 [nl/min] - 33.3 [\mu l/min])$ with an uncertainty between 8.8% and 0.25% (k=2). Measurement times range from 2 hours to 2 minutes, respectively. (2) 0.3 mg/h-1.2 mg/h mass flow of water (5-20 [nl/min]) with an uncertainty between 29.2% and 8.8% (k=2). The measurement time for this range is 2 hours. The setup consists of a pressurized liquid tank, filter, degasser, pressure sensor, DUT with control valve, balance, several temperature, and humidity sensors, and shut-off and control valves with small internal volume. All parts in the setup are connected by 1/16" OD, 0.25[mm] ID tubes. In Figure 20 a schematic of the setup is shown. It is placed on a granite table with shock absorbing blocks to reduce vibration interference from the environment. The complete setup with table is installed in a box to reduce fast temperature and humidity changes. During the measurements different temperature and humidity sensors monitor the stability of these changes. The humidity inside the box is controlled to minimize and stabilize the evaporation rate. (22.46 (44.94) T3 [*C] RH3 [% (22.93) 14 [*C] 46.38) RH4 [% Figure 20 – Schematic of Bronkhorst facility Description of The method is gravimetric and mass flow is determined using the "flying" method, which is Measurement explained below. The most important feature of the setup is that a stable flow is generated Principle using the DUT as the flow controller, which controls a piezoelectric valve. Figure 20 provides a schematic overview of the setup, and in Figure 21, a photograph of the setup is given. The piezoelectric valve is placed in front of the DUT to have a flow path between the DUT and the balance without active elements that might introduce discrepancies between the DUT and the balance. The medium that is used is extra pure deionized water that is subsequently filtered (0.5 μ m pore size) and degassed. The water is placed inside a 750-ml stainless steel tank that is pressurized at 5 [bar] using helium. Before a calibration or measurement is started, the setup is prepared to ensure a stable and pure liquid flow. "Pure liquid flow" refers to water flow without particles, i.e., larger than $0.5 \,\mu m$, and with a minimal amount of gas. The preparation is done by flushing the setup for several minutes by fully opening the piezoelectric valve and all other valves in the system before the DUT. Then the DUT is connected and flushed together with the tubing between the DUT and the balance by again fully opening the piezoelectric valve. The stability of both the DUT and the balance is checked manually, and when a stable flow is reached, the calibration or

measurement can start. The shut-off valves used in this setup are pneumatic with small internal volume and do not generate heat.



Figure 21 – Photograph of the primary standard at the Bronkhorst calibration facility.

The water that flows towards the balance is collected in a beaker via a small glass tube with its outflow positioned above a glass filter that is placed in the beaker. A constant liquid "bridge" is created during the measurements, Figure 22.



Figure 22– Weighing zone on the balance in an environment with humidity control.

The primary standard at Bronkhorst uses a high-precision balance as mass flow reference. This is implemented by differentiating its measured mass (Δm) to measured time (Δt). The sample time equals 100 ms and the calculated mass flow is filtered using a 60-s moving average. The resulting output is mass flow

(*ṁ*)

As shown in:

$$m = lim_{\Delta t \to 0} \frac{\Delta m}{\Delta t} = \frac{m_r}{t_r}$$

Where m_r and t_r are the reference mass and reference time, respectively. An RS-232 data interface is used between the balance and data acquisition. This interface combines each mass

| | sample with the correct time sample, resulting in a mass flow. This way, the flow of the DUT can be directly compared to the flow indicated by the balance, which we call the "flying" method. The uncertainties on mass and time of the balance are known and, together with the uncertainty in the applied corrections, are used to determine the total uncertainty of the setup. |
|---|---|
| Can the Facility be used for Static / Dynamic or Both? | The facility can be used for static and dynamic measurements. The main focus of the facility was to improve static measurements by improving the setup and the uncertainty budget of the gravimetric method. The dynamic measurement is based upon this method. The balance is read out at a frequency of 10 [Hz]. The largest uncertainties of low flow rate beneath 2000 [mg/h] (33.3 [μ l/min]) when measured within 60[sec] are the balance calibration and linearity uncertainties. The balance calibration uncertainty provides a worst-case approach during a dynamic measurement and will be much better in practice. To prove this, further investigation is necessary. |
| Facility Flow Ranges | For liquids: 1 g/h – 30 kg/h under ISO17025 accreditation. < 1 g/h down to 1 mg/h or less under investigation. High flows up to 1000 kg/h. |
| Temperature / Pressure Ranges | Pressure: 1 – 9 bar absolute; (for liquids) Temperature: 19 – 24 °C |
| Other Fluids | Primary fluid: ultra-pure water |
| Uncertainty Budget | Static measurements: The primary standard in the range of 1–2000 [mg/h] mass flow of water (20 [nl/min] – 33.3 [μl/min]) has an uncertainty between 0.25% and 8.8%. This setup can also be used for calibrations in the range of 0.3–1.2 [mg/h] mass flow (5–20 [nl/min]) with an uncertainty between 8.8% and 29.2%. Dynamic measurements: 1.8–6 [mg/h] mass flow of water (30–100 [nl/min]) has an uncertainty between 163% and 543%. |

5.8 – Technische Hochschule Lübeck (THL)



| | Table 3 – Acquisition resolution | | | | | | | |
|--|--|--------------------------|--|--------------------|--|--|--|--|
| | | Capillary ID | resolution [nl/px] 5.0L / 4.0L / 2.0L | Volume [µl] | | | | |
| | | 150 | 0.04 / 0.05 / 0.10 | 0.05 / 0.07 / 0.13 | | | | |
| | | 300 | 0.17 / 0.21 / 0.42 | 0.21 / 0.27 / 0.54 | | | | |
| | | 600 | 0.66 / 0.84 / 1.68 | 0.85 / 1.07 / 2.15 | | | | |
| | | 1000 | 1.84 / 2.33 / 4.66 | 2.35 / 2.98 / 5.57 | | | | |
| Description of Measurement Principle | The measurement principle is optical front tracking. The volumetric change inside a cylindrical geometry is measured with high precision by monitoring the displacement of the liquid front and the related time. The volumetric flow rate Q is determined by the displacement Δx of the liquid front during a time interval Δt and the radius R of the capillary or of the syringe. Q = (Δx / Δt) π R ² | | | | | | | |
| Can the Facility be used for Static / Dynamic or Both? | The facility can handle dynamic conditions. The volume can be determined every ms. The camera can sample 1000 frames per second. | | | | | | | |
| Facility Flow Ranges | The facility has been used between 50 nl/min and 500 $\mu l/min.$ | | | | | | | |
| Temperature / Pressure Ranges | The facility can cover only room temperature. Pressure range is limited between ambient pressure and 6 bar | | | | | | | |
| Other Fluids | Primary fluid is wa Water based solut | iter. ions could also | be used. | | | | | |
| Uncertainty Budget | Water based solutions could also be used. Uncertainty is 4% for flow rates higher than 50 nl/ min. | | | | | | | |

5.9 – TÜV SÜD National Engineering Laboratory (NEL) / University of Strathclyde (UoS)

The original plan was for NEL to complete the work in their own facility. However, the decision was made to complete the test work at University of Strathclyde's facility.



| Description of Measurement Principle | on of ment The measurement relies on tracking fluorescent beads suspended in water-based fluid approx. 21 ° C flowing into a microfluidic serpentine of known dimensions. To measure differ flow rates at approximately the same flow velocity and applied pressure values, the fl resistance of the microfluidic serpentine is varied by changing the length and width or microfluidic channel while fixing its height. The cross section of the channel is rectangular fluidic resistance is derived from Hagen-Poiseuille's law: | | | | | | |
|--|---|--|--|--|--|--|--|
| | $R_{\rm h} = \frac{12\mu L}{wh^3 \left(1 - 0.63h/w\right)}.$ | | | | | | |
| | where R_h is the fluidic resistance, μ is the dynamic viscosity, <i>L</i> is the length of the channel, <i>w</i> is the width and <i>h</i> is the height of the channel. Different values of R_h will determine the flow rate achieved inside the serpentine. | | | | | | |
| | Other options for flow measurements are available which include the use of immiscible phases. The flow rate measurements will rely on tracking a moving water/oil interface. | | | | | | |
| Can the Facility be used for Static / Dynamic or Both? | The facility can handle both steady-state and transient flow rate measurements. To achieve this, the applied pressures must be programmed to the appropriate transient values (through a software interface controlling the pressure system) or connecting a second devices which creates intermittent flow. | | | | | | |
| | Prior to each measurement, fluids are degassed to reduce air bubbles in the liquids to minimize the fluidic compliance. The walls of the microfluidic channels can be treated to become hydrophilic and low adhesion to prime water fluids, avoid air bubbles and beads adhesion to channel walls. | | | | | | |
| Facility Flow Ranges | The minimum flow rate the facility is expected to be able to measure is 5 nL/min. The maximum flow rate that has been designed to be measured, according to project specification, is at 100 nL/min. | | | | | | |
| Temperature / Pressure Ranges | The applicable full pressure range of the facility is from 30 to 1000 mbar. However, pressure values from 50 to 200 mbar will be used. Currently, the facility will be operated at room temperature (~21.7 °C). However, further measures can be implemented (such as a Peltier chamber and/or a humidity chamber) to maintain temperature and compensate liquid evaporation. | | | | | | |
| Other Fluids | The primary fluid used is distilled water (density 0.9982 g/mL at 20 °C). Any fluids (Newtonian or Non-Newtonian fluids) that are in aqueous phase can be used within the facility, e.g., blood. | | | | | | |
| Uncertainty Budget | The overall uncertainty of the flow rate measurement is calculated based on the variation in dimension of the microfluidic channel and the uncertainty of the position of the bead in each frame depending on the frame rate used. | | | | | | |
| | Because of the fabrication processes, there are variations on the dimensions of the channels. The channels will be characterized using a scanning electron microscope (SEM) and an Alpha- Step surface profiler. | | | | | | |

6 – Test procedures

The procedures detailed in *Protocol Comparison: microflow* (Activity A1.3.2) were followed for both the Static and Dynamic calibrations at each laboratory [2]. The following sub-sections provide a summary of the two calibration types.

6.1 – Static calibration

The calibration conditions were specified as follows:

- Upstream pressure: 0.5 bar to 2.5 bar
- Water temperature: Between 17 °C and 23 °C
- Minimum measurement time was dependent upon the test set up, but stable flow must be achieved before logging

For each test run, at least three repetitions per point were performed. Each laboratory decided whether to perform three single measurement test points or analyse three independent sections of a single longer measurement test point.

Table 4,

Table 5 and Table 6 summarise the test points completed at each laboratory using each of the applicable Transfer Standard devices respectively. Green means that the TS was calibrated at that test condition. Red means the TS was not calibrated at that test condition.

| Flow rate [nL/min] | IPQ | CETIAT | METAS | RISE | DTI | нs | BHT-BV | THL | UoS/NEL |
|-----------------------|-----|--------|-------|------|-----|----|--------|-----|---------|
| 1500 | | | | | | | | | |
| 1000 | | | | | | | | | |
| 500 | | | | | | | | | |
| 100 | | | | | | | | | |
| 70 | | | | | | | | | |
| 50 | | | | | | | | | |
| 20 | | | | | | | | | |

Table 4 – Flow rates completed by each flow laboratory for TS1

| Flow rate [nL/min] | IPQ | CETIAT | METAS | RISE | DTI | нs | BHT-BV | THL | UoS/NEL |
|-----------------------|-----|--------|-------|------|-----|----|--------|-----|---------|
| 1500 | | | | | | | | | |
| 1000 | | | | | | | | | |
| 500 | | | | | | | | | |
| 100 | | | | | | | | | |
| 70 | | | | | | | | | |
| 50 | | | | | | | | | |
| 20 | | | | | | | | | |

Table 5 – Flow rates completed by each flow laboratory for TS2

Table 6 – Flow rates completed by each flow laboratory for TS3

| Flow rate [nL/min] | IPQ | CETIAT | METAS | RISE | DTI | нs | BHT-BV | THL | UoS/NEL |
|-----------------------|-----|--------|-------|------|-----|----|--------|-----|---------|
| 100 | | | | | | | | | |
| 50 | | | | | | | | | |
| 20 | | | | | | | | | |
| 10 | | | | | | | | | |
| 5 | | | | | | | | | |

6.2 – Dynamic calibration

The calibration conditions were specified as follows:

- Upstream pressure: 0.5 bar to 2.5 bar
- Water temperature: Between 17 °C and 23 °C
- Minimal measurement time was dependent upon the test set up

For each test run, at least three repetitions per point were performed. The flow profile start times are shown in Table 7 below. The flow profile trend is shown in Figure 27.

| Start time [s] | Log time [s] | og time Volume flow Volume [s] [nL/min] [nL] | | Total Volume [nL] |
|-------------------|-----------------|---|----|----------------------|
| 0 | 30 | 50 | 25 | 25 |
| 30 | 30 | 80 | 40 | 65 |
| 60 | 30 100 | | 50 | 115 |
| 90 | 90 30 50 | | 25 | 140 |
| 120 | 30 30 15 | | 15 | 155 |
| 150 | 150 30 50 | | 25 | 180 |

Table 7 – Dynamic flow profile for 3 minute log time



Figure 27 – Dynamic flow profile for 3 minute log time

7 – Organization of the comparison and reference value determination

Each laboratory evaluated their own measurement uncertainty for each calibration data point. The calculations were based on standardised methods as found in the Guide to the Expression of Uncertainty in Measurement [3]. The measured data and calculated measurement uncertainties were then provided to the Pilot laboratory for the Equivalence analysis and reporting. The uncertainty procedures detailed in *Uncertainty components and methods of their evaluation* (Activity A1.2.1) were meant to be followed for both the Static and Dynamic calibrations at each laboratory [4].

In this intercomparison exercise, the individual laboratories each had different practices for estimating their measurement uncertainty. Each partner provided information on the facility measurement uncertainty over a defined range in Section 3. However, in some instances different flow ranges were covered, and the values did not include all of the potential measurement uncertainty sources. Another potential difference between the laboratories was whether the calculation included stability and repeatability or just repeatability. By incorporating different methodologies and definitions, the magnitude of measurement uncertainty for each laboratory could vary significantly.

A summary of key components of each laboratory's uncertainty calculation method is shown in Table 8 below. This table is not exhaustive and only includes three uncertainty sources. Indeed, the various components that contribute to the reference flow rate uncertainty have not been detailed and will be facility methodology dependent. The colour code for Table 8 is as follows:

Green indicates that the budget captures that uncertainty source separately. Red indicates the that the uncertainty source is not considered exclusively. For example, IPQ considers the *Repeatability* uncertainty to be captured as part of the *Reference flow rate* uncertainty.

| | Uncertainty Source | IPQ | CETIAT | METAS | RISE | DTI | HS | BHT-BV | THL | UoS/NEL |
|---|------------------------|-----|--------|-------|------|-----|----|--------|-----|---------|
| А | Reference flow rate | | | | | | | | | |
| В | Repeatability | | | | | | | | | |
| с | Stability | | | | | | | | | |

Table 8 – Facility measurement uncertainty source

To determine the reference value the formula of the weighted mean was used, using the inverses of the squares of the associated standard uncertainty as the weights [5]:

$$y = \frac{x_1/u^2(x_1) + \dots + x_n/u^2(x_n)}{1/u^2(x_1) + \dots + 1/u^2(x_n)}$$
(1)

To determine the standard deviation u(y) associated with y:

$$u(y) = \sqrt{\frac{1}{1/u^2(x_1) + \dots + 1/u^2(x_n)}}$$
(2)

To identify the overall consistency of the results a chi-square test was applied to all *n* calibration results.

$$\chi_{obs}^{2} = \frac{(x_{1} - y)^{2}}{u^{2}(x_{1})} + \cdots \frac{(x_{n} - y)^{2}}{u^{2}(x_{n})}$$
(3)

where the degrees of freedom are defined as:

$$\nu = n - 1 \tag{4}$$

The consistency check was deemed to be a pass when $\Pr(\chi^2(\nu) > \chi^2_{obs}) < 0.05$

where *Pr* is the probability. The calculations were performed in Microsoft Excel using the function CHIINV (probability, degrees, of freedom-1):

$$\chi^2_{obs} < CHIINV(0.05; v) \tag{5}$$

If the consistency check passed, then y was accepted. If it failed, then the results from the laboratory with the largest contribution to χ^2_{obs} were omitted from the evaluation and the consistency check repeated.

This enabled the comparison of the mean results of each laboratories to the weighted mean value (*REF2*), using each laboratory's uncertainty values. The equivalence of the references can be quantified by calculating the normalised deviation, or equivalence, in the form of the *En* value (*En2*) [6] [7] [8].

$$En2 = \frac{LAB - REF2}{\sqrt{(U_{95}LAB)^2 + (U_{95}DRIFT)^2 - (U_{95}REF2)^2}}$$
(6)

where REF2, U₉₅REF2 and U₉₅DRIFT are defined as:

$$U_{95}REF2 = \frac{1}{\sqrt{\sum\left(\frac{1}{(U_{95}LAB)^2}\right)}}$$
(7)

$$REF2 = \frac{\sum (LAB/(U_{95}LAB)^2)}{\sum (1/(U_{95}LAB)^2)}$$
(8)

$$U_{95}DRIFT = \frac{\Delta\varepsilon}{\sqrt{3}} \tag{9}$$

The Epsilon was calculated as the maximum deviation per flow rate at separate calibration dates. From Report *Calibration of Transfer Standards* (Activity A1.3.1), METAS performed characterisation measurements including reproducibility tests on the Sensirion SLG64-0075 [TS1] and Bronkhorst L01 [TS2] flow meters [9].

The Sensirion SLG64-0075 [TS1] was calibrated at METAS on 28.08.2020, 07.01.2021 and 14.09.2021. The maximum deviation (*Epsilon*) was 0.82 % at 20 nL/min and this value was used for the calculation of $U_{95}DRIFT$ for TS1. The resulting $U_{95}DRIFT$ value for TS1 was 0.47 % (k=2).

The Bronkhorst L01 [TS2] was calibrated at METAS on 09.12.2020, 11.12.2020 and 15.07.2021. The maximum deviation (*Epsilon*) was 0.71 % at 20 nL/min and this value was used for the calculation of $U_{95}DRIFT$ for TS2. The resulting $U_{95}DRIFT$ value for TS2 was 0.41 % (k=2).

No variability was found in the CETONI Nemesys pump [TS3], therefore the drift uncertainty was not added to the reference value for the results of the CETONI Nemesys pump [TS3].

To establish equivalence between the different laboratories, the *En* value must meet the condition of being less than 1. A warning was issued when $1 > En \le 1.2$. If the *En* value was greater than 1.2 then the results were considered inconsistent.

8 – Results of the test measurements

To avoid overwhelming the reader with numerous tables and charts, the static calibration data for Transfer Standard 1, Transfer Standard 2 and Transfer Standard 3 are presented in Appendix A, B and C respectively. The dynamic calibration data for Transfer Standard 1 and Transfer Standard 2 are presented in Appendix D and E respectively.

The following results for each Transfer Standard for each calibration method have been presented in the sub-section 6.1 and 6.2. The population size, observed chi-squared value and calculated threshold for each of the comparisons have been included.

The results have all been plotted with an artificial offset to the flow rate to aid visibility for the reader. For example, the 1500 nL/min data points were presented for each laboratory with a 45 nL/min offset ranging from 1275 nL/min to 1725 nL/min.

The uncertainty bands for each result are based upon the supplied measurement uncertainty for that calibration point and include the sources as described in Section 3 and Section 5.

The calculated Equivalence values for each laboratory are also displayed in the following sub-sections. In the Equivalence value tables, the following grading scheme was used:

- *En < 1* = pass
- 1 ≥ En ≤ 1.2 = warning and cell highlighted Amber
- En > 1.2 = fail and cell highlighted Red
- No En value = Laboratory did not conduct the experiment and cell highlighted Dark Grey
- (-) En value = Laboratory excluded after the chi-square test and cell marked with a "-" and highlighted Light Grey

8.1 – Static calibration

The static calibration results are presented below along with the weighted mean error, *REF2* below. Figure 28 displays the Sensirion flow meter [TS1] static results. To improve the resolution, Figure 29 shows the same set of data but with the chart scaled for the 20 nL/min – 100 nL/min range. Table 9 displays the Equivalence values for each laboratory for the Sensirion flow meter [TS1] static results. Table 10 displays the weighted mean error and weighted uncertainty. Table 11 displays the population size, observed chi-squared value and calculated threshold.







Figure 29 – Sensirion flow meter [TS1] static results from 20 nL/min – 100 nL/min

| Flow rate | IPQ | CETIAT | METAS | RISE | DTI | HS | THL | UoS/NEL | BHT-BV |
|-----------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|
| [nL/min] | E _n 2 |
| 1500 | 0.39 | 0.74 | 0.12 | 1.16 | 0.62 | | 0.54 | | 0.83 |
| 1000 | 0.51 | 1.21 | 0.40 | 0.70 | 0.21 | | 0.58 | | 0.79 |
| 500 | 1.03 | 0.27 | 0.61 | 0.59 | 0.01 | 0.03 | 1.42 | | 0.73 |
| 100 | 1.08 | 0.10 | 0.41 | 0.96 | 0.43 | 0.06 | 0.20 | 0.87 | 0.25 |
| 70 | 0.86 | - | 0.37 | 0.95 | 0.20 | 0.10 | - | 0.28 | 0.07 |
| 50 | 0.81 | 0.03 | 0.31 | 0.49 | 0.45 | | - | - | 0.07 |
| 20 | 0.63 | - | 0.22 | 0.14 | 0.24 | | 0.25 | 0.55 | 0.06 |

Table 9 – Laboratory En values for the Sensirion flow meter [TS1] static results

| | Table 10 – Weighted mean | error and weighted up | ncertainty for the Se | ensirion flow meter | [TS1] | static results |
|--|--------------------------|-----------------------|-----------------------|---------------------|-------|----------------|
|--|--------------------------|-----------------------|-----------------------|---------------------|-------|----------------|

| Flow rate | Weighted mean error | Weighted uncertainty |
|-----------|------------------------|----------------------|
| [nr/min] | REF2 | U95REF2 |
| 1500 | 1.67 | 0.18 |
| 1000 | 1.45 | 0.21 |
| 500 | 1.25 | 0.25 |
| 100 | 2.14 | 0.46 |
| 70 | 2.64 | 0.57 |
| 50 | 2.25 | 0.65 |
| 20 | 1.04 | 0.84 |

| Flow rate | Population size | Observed chi- squared value | Calculated threshold |
|-----------|-----------------|--------------------------------|-------------------------|
| נחבי הוחן | n-1 | χ^2_{obs} | $\chi^2(n-1)$ |
| 1500 | 6 | 3.66 | 12.59 |
| 1000 | 6 | 3.84 | 12.59 |
| 500 | 7 | 5.79 | 14.07 |
| 100 | 8 | 9.45 | 15.51 |
| 70 | 6 | 4.29 | 12.59 |
| 50 | 5 | 3.00 | 11.07 |
| 20 | 6 | 10.33 | 12.59 |

Table 11 – Population size, observed chi-squared value and calculated threshold for the Sensirion flow meter [TS1] static results

Figure 30 displays the Bronkhorst flow meter [TS2] static results. To improve the resolution, Figure 31 shows the same set of data but with the chart scaled for the 20 nL/min – 100 nL/min range. Table 12 displays the Equivalence values for each laboratory for the Bronkhorst flow meter [TS2] static results. Table 13 displays the weighted mean error and weighted uncertainty. Table 14 displays the population size, observed chi-squared value and calculated threshold.



Figure 30 - Bronkhorst flow meter [TS2] static results



Figure 31 – Bronkhorst flow meter [TS2] static results from 20 nL/min – 100 nL/min

| Flow rate | IPQ | CETIAT | METAS | RISE | DTI | HS | THL | UoS/NEL | BHT-BV |
|-----------|------|--------|-------------|-------------|------|------|------|---------|---------------------|
| [nL/min] | En2 | En2 | En 2 | En 2 | En2 | En2 | En2 | En2 | E n 2 |
| 1500 | 1.11 | 0.18 | 0.06 | 0.14 | 0.27 | 0.18 | 0.02 | | 0.65 |
| 1000 | 0.65 | 0.59 | 0.47 | 0.74 | 0.67 | 0.06 | 0.04 | | 0.27 |
| 500 | 0.28 | 1.06 | 0.17 | 0.35 | 0.84 | 0.03 | 0.93 | | 0.63 |
| 100 | 0.05 | 0.19 | 0.34 | 1.04 | 0.19 | 0.37 | 1.39 | | 0.72 |
| 70 | 1.06 | 0.58 | 0.46 | 0.02 | 0.01 | 0.06 | - | 0.14 | 0.61 |
| 50 | 1.11 | 0.11 | 0.40 | 0.08 | | | - | 0.40 | 0.46 |
| 20 | 0.94 | 0.20 | 0.48 | 0.01 | | | - | - | 0.40 |

| Table 12 – Laborator | y En values for | the Bronkhorst flov | v meter [TS2] | static results |
|----------------------|-----------------|---------------------|---------------|----------------|
|----------------------|-----------------|---------------------|---------------|----------------|

Table 13 – Weighted mean error and weighted uncertainty for the Bronkhorst flow meter [TS2] static results

| Flow rate | Weighted mean error | Weighted uncertainty |
|-----------|------------------------|-------------------------|
| [[]] | REF2 | U95REF2 |
| 1500 | -0.29 | 0.12 |
| 1000 | -0.94 | 0.21 |
| 500 | -1.71 | 0.27 |
| 100 | -4.46 | 0.47 |
| 70 | -4.98 | 0.62 |
| 50 | -5.31 | 0.62 |
| 20 | -5.32 | 0.87 |

Table 14 – Population size, observed chi-squared value and calculated threshold for the Bronkhorst flow meter [TS2] static results

| Flow rate | Population size | Observed chi- squared value | Calculated threshold |
|-----------|-----------------|--------------------------------|-------------------------|
| [nL/min] | n-1 | χ^2_{obs} | $\chi^2(n-1)$ |
| 1500 | 7 | 3.99 | 14.07 |
| 1000 | 7 | 2.34 | 14.07 |
| 500 | 7 | 3.50 | 14.07 |
| 100 | 7 | 12.31 | 14.07 |
| 70 | 7 | 4.29 | 14.07 |
| 50 | 5 | 5.68 | 11.07 |
| 20 | 4 | 4.07 | 9.49 |

Figure 32 displays the CETONI Nemesys syringe pump [TS3] static results.

Table 15 displays the Equivalence values for each laboratory for the CETONI Nemesys syringe pump [TS3] static results. Table 16 displays the weighted mean error and weighted uncertainty. Table 17 displays the population size, observed chi-squared value and calculated threshold.



Figure 32 – CETONI Nemesys Syringe pump [TS3] static results

| Flow rate | IPQ | CETIAT | METAS | RISE | DTI | HS | THL | UoS/NEL | BHT-BV |
|-----------|------|------------------|-------|------|------------------|-----|------|---------|--------|
| [nL/min] | En2 | E _n 2 | En2 | En2 | E _n 2 | En2 | En2 | En2 | En2 |
| 100 | 0.64 | 0.31 | 1.00 | 0.57 | 1.25 | | - | | 0.23 |
| 50 | 0.37 | 0.70 | 1.31 | 0.82 | 1.13 | | - | | 0.001 |
| 20 | 0.64 | 0.04 | 0.70 | 0.13 | 0.58 | | - | | 0.22 |
| 10 | 0.64 | 0.58 | | 0.13 | | | 0.36 | | 0.28 |
| 5 | 0.13 | - | | 0.26 | | | 0.34 | | 0.18 |

Table 15 – Laboratory *En* values for the CETONI Nemesys Syringe pump [TS3] static results

Table 16 – Weighted mean error and weighted uncertainty for the CETONI Nemesys syringe pump [TS3] static results

| Flow rate | Weighted mean error | Weighted uncertainty |
|-----------|------------------------|-------------------------|
| [| REF2 | U95REF2 |
| 100 | -0.71 | 0.42 |
| 50 | -0.41 | 0.45 |
| 20 | -0.61 | 0.75 |
| 10 | -1.09 | 1.98 |
| 5 | -0.03 | 2.35 |

Table 17 – Population size, observed chi-squared value and calculated threshold for the CETONI Nemesys syringe pump [TS3] static results

| Flow rate | Population size | Observed chi- squared value | Calculated threshold |
|-----------|-----------------|--------------------------------|-------------------------|
| [nt/min] | n-1 | χ^2_{obs} | $\chi^2(n-1)$ |
| 100 | 5 | 3.97 | 11.07 |
| 50 | 5 | 4.95 | 11.07 |
| 20 | 5 | 3.40 | 11.07 |
| 10 | 4 | 5.99 | 9.49 |
| 5 | 3 | 2.64 | 7.81 |

8.2 – Dynamic calibration

The dynamic calibration results are presented below along with the weighted mean error, *REF2* below. Figure 33 displays the Sensirion flow meter [TS1] dynamic results. To improve the resolution, Figure 34 shows the same set of data but with the chart scaled for the -25 % to +25% Error range. Table 18 displays the Equivalence values for each laboratory for the Sensirion flow meter [TS1] dynamic results. Table 19 displays the weighted mean error and weighted uncertainty. Table 20 displays the population size, observed chi-squared value and calculated threshold.



Figure 33 – Sensirion flow meter [TS1] dynamic results



Figure 34 – Sensirion flow meter [TS1] dynamic results with reduced scale Y axis

Table 18 – Laboratory En values for the Sensirion flow meter [TS1] dynamic results

| Dynamic | IPQ | CETIAT | METAS | RISE | DTI | HS | THL | UoS/NEL | BHT-BV |
|---------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|
| Flow | E _n 2 |
| | | 0.50 | 0.50 | | | | | | 0.004 |

Table 19 – Weighted mean error and weighted uncertainty for the Sensirion flow meter [TS1] dynamic results

| Dynamic Flow | Weighted mean error | Weighted uncertainty |
|--------------|------------------------|-------------------------|
| | REF2 | U95REF2 |
| | 2.06 | 1.99 |

Table 20 – Population size, observed chi-squared value and calculated threshold for the Sensirion flow meter [TS1] dynamic results

| Dynamic Flow | Population size | Observed chi- squared value | Calculated threshold |
|--------------|-----------------|--------------------------------|-------------------------|
| | n-1 | χ^2_{obs} | $\chi^2(n-1)$ |
| | 2 | 1.79 | 5.99 |

Figure 35 displays the Bronkhorst flow meter [TS2] dynamic results. To improve the resolution, Figure 36 shows the same set of data but with the chart scaled for the -25 % to +25% Error range. Table 21 displays the Equivalence values for each laboratory for the Bronkhorst flow meter [TS2] dynamic results. Table 22 displays the weighted mean error and weighted uncertainty. Table 23 displays the population size, observed chi-squared value and calculated threshold.



Figure 35 – Bronkhorst flow meter [TS2] dynamic results



Figure 36 – Bronkhorst flow meter [TS2] dynamic results with reduced scale Y axis

Table 21 – Laboratory En values for the Bronkhorst flow meter [TS2] dynamic results

| Dynamic | IPQ | CETIAT | METAS | RISE | DTI | HS | THL | UoS/NEL | BHT-BV |
|---------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|
| Flow | E _n 2 |
| | | 0.03 | 0.03 | | | | | | 0.001 |

Table 22 – Weighted mean error and weighted uncertainty for the Bronkhorst flow meter [TS2] dynamic results

| Dynamic Flow | Weighted mean error | Weighted uncertainty |
|--------------|------------------------|-------------------------|
| | REF2 | U95REF2 |
| | -5.25 | 2.00 |

Table 23 – Population size, observed chi-squared value and calculated threshold for the Bronkhorst flow meter [TS2] dynamic results

| Dynamic Flow | Population size | Observed chi- squared value | Calculated threshold |
|--------------|-----------------|--------------------------------|-------------------------|
| | n-1 | χ^2_{obs} | $\chi^2(n-1)$ |
| | 2 | 0.01 | 5.99 |

9 – Conclusions

The overall conclusion from this comparison exercise was that it was extremely successful and enabled the partners to share knowledge, improve their methodologies, evaluate their measurement uncertainties, and enhance their calibrations facilities. All participants succeeded in performing the evaluation with at least one Transfer Standard at several flow rates and to obtain results in line with the agreed protocol.

The following two sub-sections provide the overall conclusions for the static calibration comparison and the dynamic calibration comparison.

9.1 – Static calibration

The results from the static calibrations were extremely promising and several laboratories achieved equivalency for at least two of the flow rates conducted with each of the three transfer standards. Specifically:

- The transfer standards used were found to demonstrate the required stability and repeatability
- 79% of calibration points with TS1 were recorded by the laboratories. 90% of the recorded calibration points with TS1 had an *En* value less than 1.0
- 81% of calibration points with TS2 were recorded by the laboratories. 88% of the recorded calibration points with TS2 had an *En* value less than 1.0
- 60% of calibration points with TS3 were recorded by the laboratories. 85% of the recorded calibration points with TS3 had an *En* value less than 1.0
- Some of the measurement uncertainty values claimed by the laboratories at certain flow rates might require further investigation
- It was possible to measure flow rates down to 5 nL/min with 3 % uncertainty.

9.2 – Dynamic calibration

The results from the dynamic calibrations validate the traceability of the three laboratories that participated in the comparison. Whilst only three laboratories conducted the comparison for dynamic flow with both of the Transfer Standards, the results were extremely positive and further underpin the laboratory measurement uncertainty. All of the calculated *En* values were less than 1.0 for the dynamic flow calibrations.

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Appendix A – Static Results Sensirion flow meter [TS1]

| Flow | IP | Q | CET | TAT | ME | TAS | RI | SE | D | TI | н | S | BH1 | ſ-BV | TI | HL | UoS, | /NEL |
|------------------|--------------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|--------------|--------------------|-----------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|
| rate [nL/min] | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) |
| 1500 | 0.85 | 2.07 | 0.67 | 1.29 | 1.74 | 0.38 | 0.90 | 0.50 | 1.26 | 0.51 | | | 2.10 | 0.28 | 1.08 | 1.00 | | |
| 1000 | 2.53 | 2.07 | 0.07 | 1.06 | 1.69 | 0.40 | 0.99 | 0.50 | 1.31 | 0.51 | | | 1.92 | 0.42 | 0.91 | 0.84 | | |
| 500 | 3.58 | 2.23 | 1.79 | 2.01 | 1.63 | 0.48 | 0.87 | 0.50 | 1.24 | 0.54 | 1.52 | 10.19 | 1.88 | 0.77 | -0.08 | 0.85 | | |
| 100 | 5.06 | 2.70 | 2.61 | 4.82 | 2.39 | 0.60 | 1.17 | 1.00 | 1.59 | 1.25 | 0.71 | 24.21 | 3.14 | 4.01 | -0.01 | 10.55 | 6.95 | 5.51 |
| 70 | 5.03 | 2.78 | 7.29 | 0.92 | 2.87 | 0.69 | 1.25 | 1.50 | 2.33 | 1.61 | 4.38 | 16.57 | 2.29 | 4.75 | -4.67 | 2.54 | 0.48 | 7.60 |
| 50 | 4.78 | 3.14 | 1.91 | 9.84 | 2.44 | 0.75 | 1.30 | 2.00 | 1.31 | 2.14 | | | 2.80 | 7.65 | -6.97 | 2.48 | -6.42 | 7.50 |
| 20 | 4.27 | 5.18 | -14.03 | 27.52 | 0.91 | 0.92 | 1.38 | 2.50 | -0.34 | 5.89 | | | 2.11 | 18.59 | -5.44 | 25.89 | 12.38 | 20.63 |

Table 24 – Measurement data for each flow laboratory for TS1

Appendix B – Static Results Bronkhorst flow meter [TS2]

| Flow | IP | Q | CET | TAT | ME | TAS | RI | SE | D | TI | н | S | BH1 | -BV | ТІ | HL | UoS | /NEL |
|------------------|--------------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|--------------|--------------------|-----------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|
| rate [nL/min] | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) |
| 1500 | -3.3 | 2.7 | -0.22 | 0.15 | -0.26 | 0.48 | -0.38 | 0.50 | -0.09 | 0.65 | -1.25 | 5.22 | -0.62 | 0.32 | -0.28 | 1.02 | | |
| 1000 | -2.4 | 2.2 | -0.53 | 0.61 | -0.65 | 0.51 | -1.40 | 0.50 | -0.38 | 0.77 | -0.30 | 10.12 | -1.08 | 0.34 | -0.91 | 0.78 | | |
| 500 | -2.6 | 3.1 | -0.99 | 0.60 | -1.60 | 0.58 | -1.91 | 0.50 | -0.59 | 1.29 | -2.08 | 11.31 | -2.13 | 0.60 | -2.75 | 1.09 | | |
| 100 | -4.6 | 2.1 | -4.65 | 1.03 | -4.69 | 0.71 | -3.44 | 1.00 | -3.27 | 6.34 | -1.20 | 8.88 | -5.65 | 1.67 | 1.96 | 4.63 | | |
| 70 | -2.9 | 2.0 | -3.33 | 2.91 | -5.28 | 0.80 | -4.95 | 1.50 | -5.08 | 8.54 | -5.81 | 14.57 | -6.41 | 2.40 | 5.58 | 2.91 | -6.61 | 11.58 |
| 50 | -2.6 | 2.5 | -5.20 | 1.18 | -5.61 | 0.86 | -5.16 | 2.00 | | | | | -6.83 | 3.32 | 6.67 | 4.82 | -10.09 | 12.05 |
| 20 | -2.7 | 2.9 | -7.29 | 9.89 | -5.63 | 1.00 | -5.30 | 2.50 | | | | | -8.49 | 8.05 | 34.52 | 9.23 | 7.94 | 15.09 |

Table 25 – Measurement data for each flow laboratory for TS2

Appendix C – Static Results CETONI Nemesys syringe pump [TS3]

| Flow | IP | Q | CET | TAT | ME | TAS | RI | SE | D | TI | н | IS | ВНТ | -BV | ТІ | HL | UoS | /NEL |
|------------------|--------------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|--------------|--------------------|-----------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|
| rate [nL/min] | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) |
| 100 | 0.02 | 1.21 | -0.53 | 0.70 | -1.29 | 0.72 | -1.52 | 1.48 | 1.30 | 1.66 | | | -1.37 | 2.9 | 16.54 | 3.52 | | |
| 50 | 0.01 | 1.21 | -0.09 | 0.64 | -1.51 | 0.95 | -1.88 | 1.86 | 1.62 | 1.85 | | | -0.41 | 5.6 | 49.83 | 20.42 | | |
| 20 | 0.00 | 1.22 | -1.21 | 14.21 | -1.11 | 1.04 | -0.95 | 2.73 | 3.03 | 6.35 | | | 2.52 | 13.9 | 16.24 | 15.38 | | |
| 10 | 0.04 | 2.65 | -7.53 | 11.35 | | | -1.53 | 3.86 | | | | | -5.24 | 14.8 | -2.94 | 5.47 | | |
| 5 | 0.15 | 2.69 | 28.48 | 51.73 | | | -1.25 | 5.26 | | | | | -5.57 | 31.3 | 4.11 | 12.53 | | |

Table 26 – Measurement data for each flow laboratory for TS3

Appendix D – Dynamic Results Sensirion flow meter [TS1]

| | IP | Q | CET | ΠΑΤ | ME | TAS | RI | SE | D | TI | н | IS | BH1 | -BV | TI | IL | UoS | /NEL |
|-----------------|--------------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|--------------|--------------------|-----------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|
| Dynamic Flow | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) |
| | | | -1.39 | 7.11 | 2.35 | 2.1 | | | | | | | 0.57 | 400.76 | | | | |

| Table 27 – D | ynamic test com | pleted by | each flow | laboratory | for TS1 |
|--------------|-----------------|-----------|-----------|------------|---------|
| | | | | | |

Appendix E – Dynamic Results Bronkhorst flow meter [TS2]

| | IP | ٩Q | CET | ΠΑΤ | ME | TAS | RI | SE | D | TI | F | IS | BHT | ſ-BV | Т | HL | UoS | /NEL |
|-----------------|--------------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|--------------|--------------------|-----------|--------------------|-----------|--------------------|--------------|--------------------|--------------|--------------------|
| Dynamic Flow | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) | Error (%) | Uncertainty (%) |
| | | | -5.02 | 8.66 | -5.27 | 2.06 | | | | | | | -4.74 | 400.77 | | | | |

| Table 28 – Dy | namic test co | mpleted b | v each flow | laborator | v for TS2 |
|---------------|---------------|------------|----------------|-----------|-----------|
| 1001020 0 | | inpicted b | y cucii 110 11 | laborator | y 101 132 |